

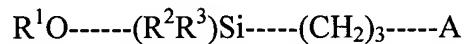
**AMENDMENTS TO THE CLAIMS**

This listing of claims will replace all prior versions, and listings, of claims in the application.

**Listing of Claims:**

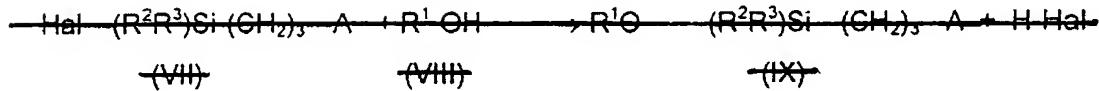
1-19 (Canceled)

20. (Currently amended) A continuous process for preparing an organodialkylalkoxysilane of formula (IX):



Comprising the steps of:

a) continuously contacting an alcohol of formula (VIII):  $R^1-OH$  in countercurrent with a silane of formula (VII):  $Hal---(R^2R^3)Si-(CH_2)_3---A$ ,  
in order to carry out the alcoholysis reaction of said silane according to the following reaction in order to obtain the silane of formula (IX) and a product of formula H-Hal,



the operation being carried out with stripping of the product of formula H-Hal formed,  
and

b) recovering the organodialkylalkoxysilane formed in the reactor, in which formulae

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the symbol Hal represents a halogen atom selected from chlorine, bromine and iodine atoms, the chlorine atom being preferred;

the symbols R<sup>1</sup>, which are identical or different, each represent a monovalent hydrocarbon group selected from a linear or branched alkyl radical having 1 to 15 carbon atoms and a linear or branched alkoxyalkyl radical having 2 to 8 carbon atoms; the symbols R<sup>2</sup> and R<sup>3</sup>, which are identical or different, each represent a monovalent hydrocarbon group selected from a linear or branched alkyl radical having 1 to 6 carbon atoms and a phenyl radical; and

A represents a removable group selected alternatively from: a halogen atom Hal belonging to chlorine, bromine and iodine atoms, or a radical para-R<sup>0</sup>-C<sub>6</sub>H<sub>4</sub>-SO<sub>2</sub>-O- wherein R<sup>0</sup> is a linear or branched C1-C4 alkyl radical, or a radical R<sup>0</sup>-SO<sub>2</sub>-O- wherein R<sup>0</sup> is as defined above, or a radical R<sup>0</sup>-CO-O- wherein R<sup>0</sup> is as defined above.

21. (Previously presented) The process according to claim 1, wherein within the reactor a descending liquid fluid comprising the silane of formula (VII) and an ascending gaseous fluid comprising the alcohol of formula (VIII) will circulate in countercurrent.

22. (Previously presented) The process according to claim 20, wherein the alcoholysis reaction is carried out within the reactor at a temperature between the boiling temperature of the alkanol of formula (VIII) and the boiling temperature of the starting silane of formula (VII), the reaction being carried out in the reactor alternatively at atmospheric pressure or at reduced pressure or at superatmospheric pressure.

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23. (Previously presented) The process according to claim 23, wherein the silane of formula (VII) is 3-chloropropyldimethylchlorosilane, Hal and A are chlorine and the alcohol of formula (VIII) is ethanol.

24. (Previously presented) The process according to claim 23, wherein the 3-chloropropyldimethylchlorosilane, is introduced in the upper part of the reactor, the ethanol in the lower part, the reaction temperature in the column is greater than 77.80°C and less than 178°C at atmospheric pressure and the hydrochloric acid formed is stripped by the ethanol.

25. (Previously presented) The process according to claim 20, wherein the reaction is carried out in the presence of an organic solvent or an inert gas, said solvent having a boiling temperature at the operating pressure which is between the boiling temperature of the ethanol of formula (VIII) and that of the silane of the formula (VII).

26. (Previously presented) The process according to claim 25, wherein the solvent is toluene, monochlorobenzene or xylene and the products corresponding to formulae (I) to (XI) have ethyl groups R<sup>1</sup> and methyl groups R<sup>2</sup> and R<sup>3</sup> and A and Hal represent a chlorine atom.

27. (Previously presented) The process according to claim 20, wherein the pressure inside the reactor is less than atmospheric pressure, atmospheric pressure or greater than atmospheric pressure.

28. (Previously presented) The process according to claim 20, wherein the alcohol/silane molar ratio is greater than 1.

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29. (Previously presented) The process according to claim 20, wherein the countercurrent reactor consists of a column equipped in its internal structure with a dumped or ordered packing or with plates.

30-38. (Canceled)